

no mixing losses yields COP values not much less than the Carnot values. Once mixing losses are allowed to affect the results, using either an ideal gas model or a real gas model, the COP values drop markedly due to the internal irreversibilities or lost work. Hamner also reports experimental data on such an ejector-operated refrigeration cycle, rated at approximately one ton of refrigeration and employing R-11 as the refrigerant. Experimental COP values of about 0.10 to 0.25 were obtained for pressure ratios (P_s/P_c) of 5.0 to 7.5.

CONCLUSIONS

This article has demonstrated the applicability of the HYSYS computer-aided process design system to the simulation and analysis of a solar-powered refrigeration cycle. While such a cycle consists of a number of standard chemical process equipment items such as heat exchangers, a pump, and an expansion valve, the key hardware element in this cycle is a thermal compressor or jet ejector. Models of the latter item, while a relatively common piece of processing equipment in the chemical and allied industries, are not that extant in computer-aided process design systems such as HYSYS or comparable software packages. The employment of an adjust or control module to balance the work of a compressor and an expander in a cycle was illustrated in this work.

The coefficient of performance (COP) values for refrigeration cycles driven by a solar collector and jet ejector are admittedly much smaller than those of conventional cycles employing mechanical compressors. As numerous authors^[1-3] have pointed out, however, applications of the former may be economical in cases wherein the required input heat is very inexpensive (e.g., solar energy) or it would be otherwise wasted, as from the cooling system of an automobile engine. And there are certainly more than just technological factors operative in this arena.^[4] Lastly, it should be remembered that the energy input to a mechanical vapor-compression refrigeration cycle generally originates from an electrical power plant. This power often derives from the combustion of a fuel with a process efficiency of about 33%. Thus,

the ultimate amount of energy required in such a mechanical cycle is roughly three times the amount actually supplied to the compressor.

NOTE FROM OCTAVE LEVENSPIEL

I have written a little book especially designed for the first engineering thermo course. It is called

Understanding Engineering Thermo

and it uses a radically different teaching approach. Students like it.

The OSU Bookstore (Box 489, Corvallis OR 97339) is distributing it at \$20 plus mailing cost. If you are a thermo teacher and want a desk copy, contact me at

Chemical Engineering Department
Gleeson 103
Oregon State University
Corvallis OR 97331

Octave Levenspiel
octave@che.orst.edu

Perhaps the major contribution of this work is of a pedagogical nature. Thus, this study of a solar-powered refrigeration cycle, exploring different refrigerants, efficiencies, operating conditions, etc., could represent an excellent computer-aided design project in an introductory engineering thermodynamics course. It is in this spirit that this study was formulated.

REFERENCES

1. Heymann, M., and W. Resnick, "Optimum Ejector Design for Ejector-Operated Refrigeration Cycles," *Israel J. Technol.*, **2**, 242 (1964)
2. Hamner, R.M., "An Alternate Source of Cooling: The Ejector-Compression Heat Pump," *ASHRAE J.*, **22**(7), 62 (1980)
3. Chen, L.-T., "A Heat Driven Mobile Refrigeration Cycle Analysis," *Energy Conserv.*, **18**, 25 (1978)
4. Pavone, T., and G. Patrick, "Energy Tax Credit Aids Investment Projects," *Chem. Eng.*, **88**(4), 99 (1981)
5. Khoury, F., M. Heyman, and W. Resnick, "Performance Characteristics of Self-Entrainment Ejectors," *I&EC Proc. Des. Develop.*, **6**, 331 (1967)
6. DeFrate, L.A., and A.E. Hoerl, "Optimum Design of Ejectors Using Digital Computers," *Chem. Eng. Prog. Symp. Series*, **55**(21), 43 (1959)
7. Holldorff, H.F.W., J.D. Muzzy, and J.T. Sommerfeld, "Digital Computer Model of a Thermal Compressor," *Proc. 1981 Summer Computer Simulation Conf.*, p. 247, July (1981)
8. Seader, J.D., W.D. Seider, and A.C. Pauls, *FLOWTRAN Simulation: An Introduction*, 2nd ed., The CACHE Corp., Cambridge, MA (1977)
9. Clark, J.P., T.P. Koehler, and J.T. Sommerfeld, *Exercises in Process Simulation Using FLOWTRAN*, 2nd ed., The CACHE Corp., Salt Lake City, UT (1980)
10. *PRO/II Keyword Input Manual*, Version 4.0, Simulation Sciences, Inc., Brea, CA (Sept. 1994)
11. *HYSIM: Special Features and Application Guide*, Version C2.50, Hyprotech, Calgary, Canada (March, 1994)
12. Kyle, B.G., *Chemical and Process Thermodynamics*, 2nd ed., Prentice Hall, Englewood Cliffs, NJ (1992) □

TABLE 8

Influence of Heat Rejection Temperature (T_0) on COP and Efficiency Values ($T_R = 40^\circ\text{F}$, $T_S = 200^\circ\text{F}$)

Rejection Temperature (T_0), °F	Refrigeration Cycle (COP_c)	Efficiency of heat engine (E_c)	Overall cycle COP [$=\text{COP}_c(E_c)$]
125	5.882	0.1136	0.6684
110	7.143	0.1364	0.9740
100	8.333	0.1515	1.2626
90	10.000	0.1667	1.6667
77	13.514	0.1864	2.5184